



Application

Low-pressure steam exhaust from industrial operations such as evaporators or cookers is usually vented to the atmosphere or condensed in a cooling tower. Simultaneously, other plant operations may require intermediate-pressure steam at 20 to 25 PSIG. Instead of letting down high-pressure steam across a throttling valve to meet these needs, low-pressure waste steam can be mechanically compressed or boosted to a higher pressure so that it can be reused.

Vapor recompression involves incorporating a blower to increase the temperature of the latent heat in steam to render it usable for process duties. Recompression with a blower requires only a small fraction of the energy required to raise an equivalent amount of steam in a boiler.

Example

Consider a petrochemical plant that vents 8 PSIG steam to the atmosphere. At the same time, a process imposes a continuous requirement on the boiler for approximately 5,300 pounds per hour (lb/hr) of 23 PSIG steam. A Tuthill M-D Pneumatics™ 9012 PD Plus blower operating at 2100 RPM, 143 BHP (107 kW) accomplishes this task. In addition, approximately 0.6 GPM of 80° F condensate is injected into the blower to eliminate superheating of the steam, resulting in an additional 297 lb/hr of steam to the heating process.

Assuming electricity cost of \$0.08/kWh, energy cost for the blower is calculated as follows:

$$143 \text{ BHP} \times 0.7457 \times 8760 \text{ hr/yr} \times \$0.08/\text{kWh} = \$74,730$$

If an equivalent quantity of 23 PSIG steam (enthalpy for saturated steam at 37.7 PSIA is 1159 BTU/lb) were to be supplied by an 80% efficient naturalgas-fired boiler, the steam production costs with fuel priced at \$8.00 per million Btu (\$8.00/MMBtu) and 70°F feed water (enthalpy is 38 Btu/lb) are:

$$(5297 \text{ lb/hr} \times (1159-38) \text{ BTU/lb} \times 8760 \text{ hr/yr} \times \$8.00/\text{MMBTU}) / 0.8 \times 10^{-6} = \$520,163$$

Annual energy savings by recompression:
\$520,957 – 74,730 = \$445,433 SAVINGS

MTE (Metric Tons Equivalent) CO₂ greenhouse gas emission savings:

Average pounds of CO₂ produced to generate 1.00 kWh = 1.341

$$\text{Blower: } 143 \text{ BHP} \times 0.7457 \times 8760 \text{ hr/yr} \times 1.341 = 1252660 \text{ lbs.}$$

$$1252660 / 2204.62 = 568.2 \text{ MTE CO}_2$$

Average pounds of CO₂ produced by combustion of 1 MMBTU Natural Gas = 117.08

$$\text{Boiler: } ((5297 \times (1159-38) \times 8760) / 0.8) \times 10^{-6} \times 117.08 = 7810646 \text{ lbs.}$$

$$7810646 / 2204.62 = 3453 \text{ MTE CO}_2$$

Annual greenhouse gas emissions savings by recompression:
3453 MTE CO₂ - 568.2 = 2884.8 MTE CO₂ SAVINGS



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